



# **Flue-Gas Water as a Resource for Carbon-Capturing Power- Plants**

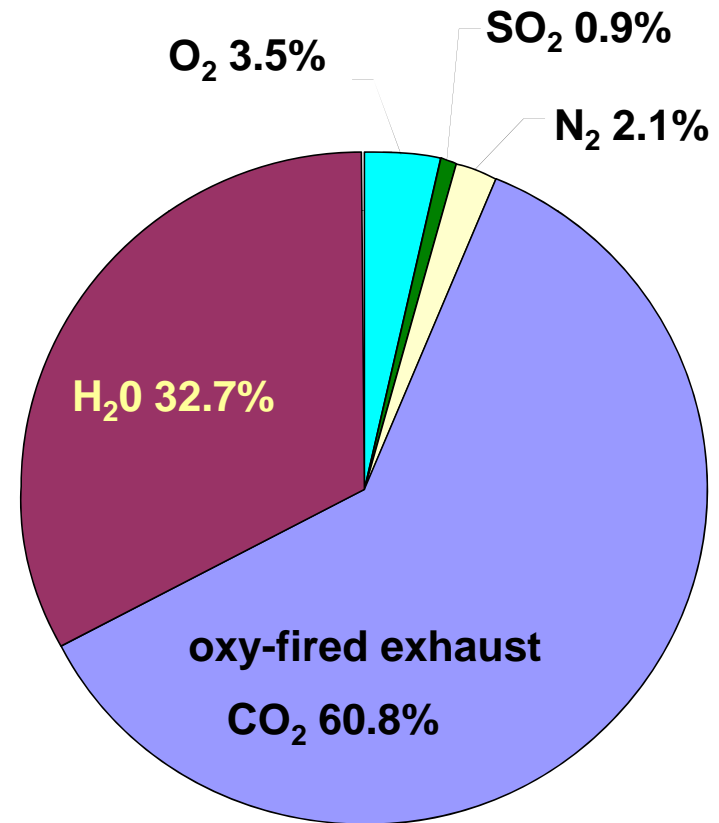
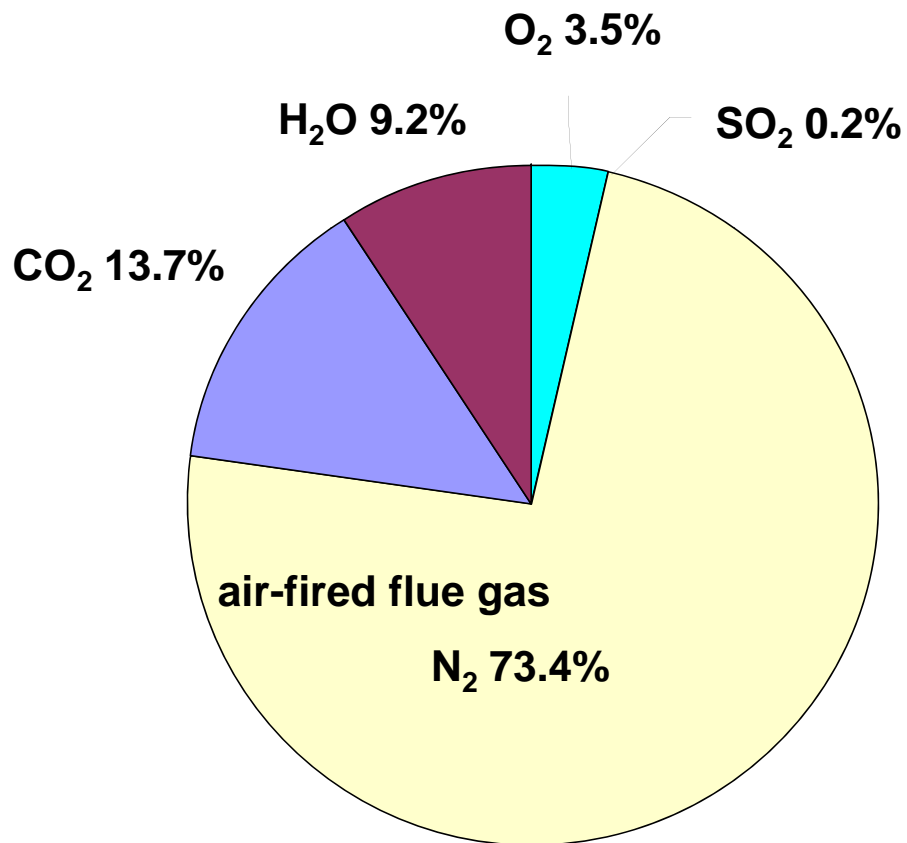
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# Basic Process Outline

- Combust fuel in directly-supplied (not air-carried) oxygen.
  - Undiluted products of combustion
- Capture combustion products to capture the CO<sub>2</sub> component
- Cooling and compression (part of the capture process) produce condensed flue-gas water

# Combustion Products

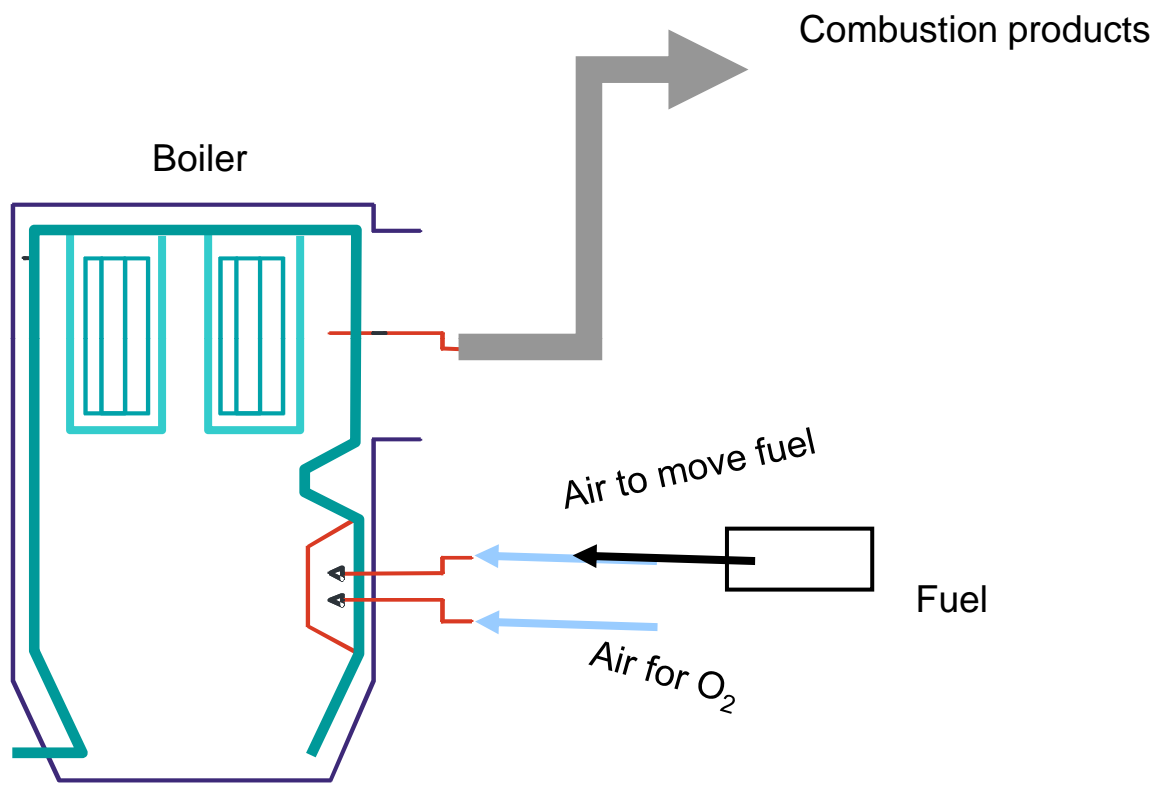
air-firing                      oxy-firing



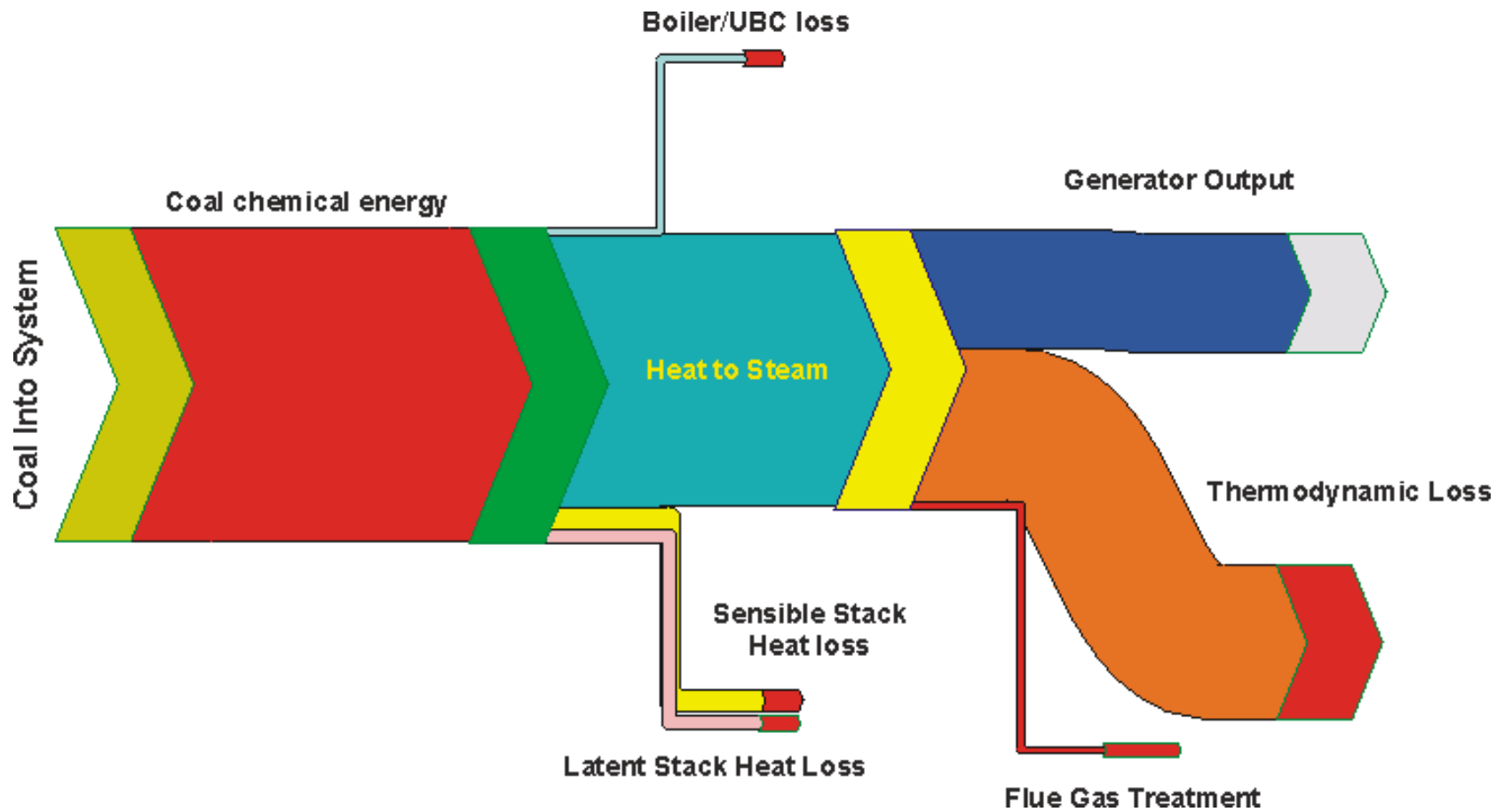
# Water/energy: The Oxy-Combustion with Integrated **P**ollutant **R**emoval (IPR) effort

- Water previously released to the atmosphere now presents a resource
  - Energy (heat recovery)
  - Heat-exchange medium
  - Combustion-optimization (completion of combustion)

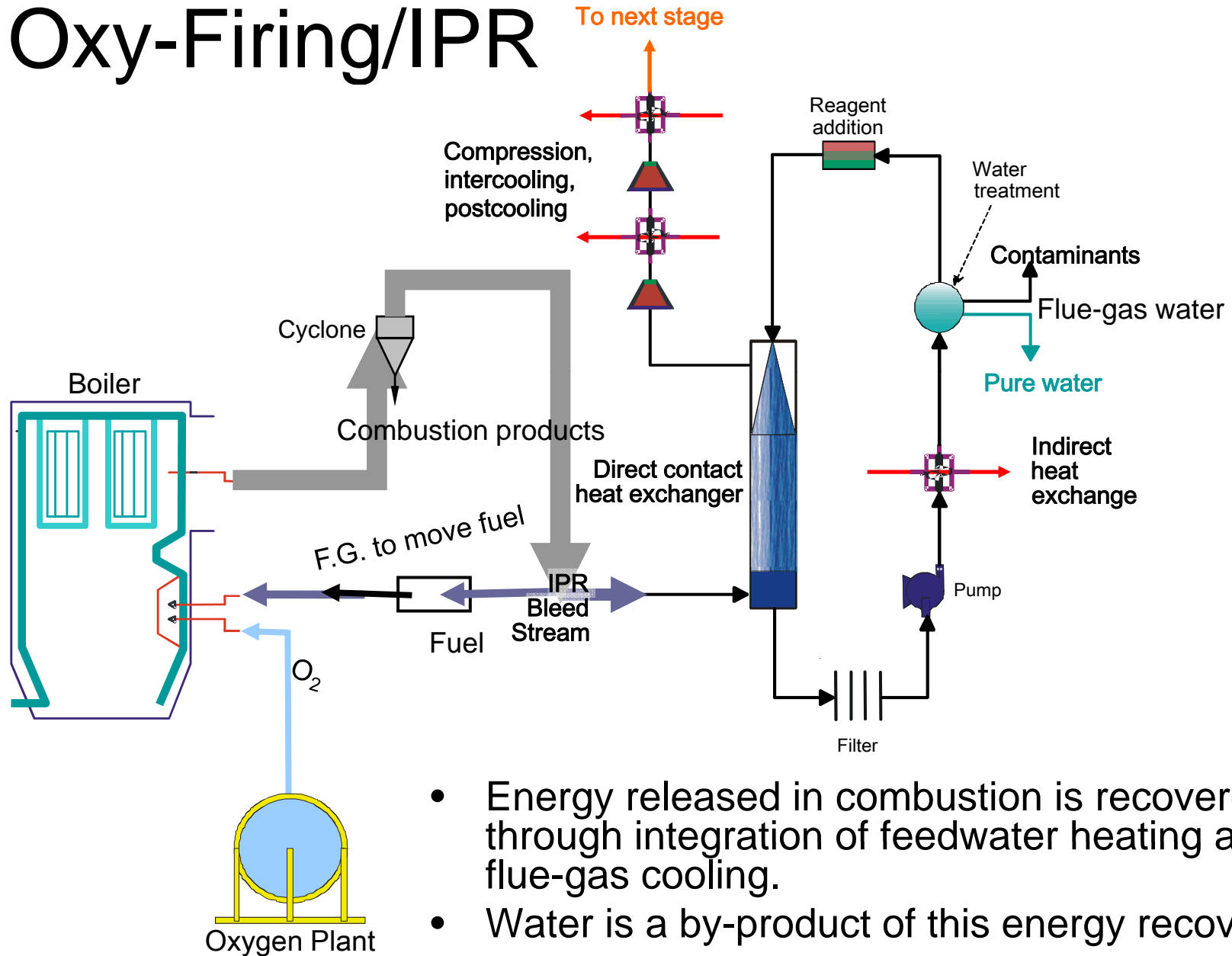
# Air-Firing



# Air-Firing

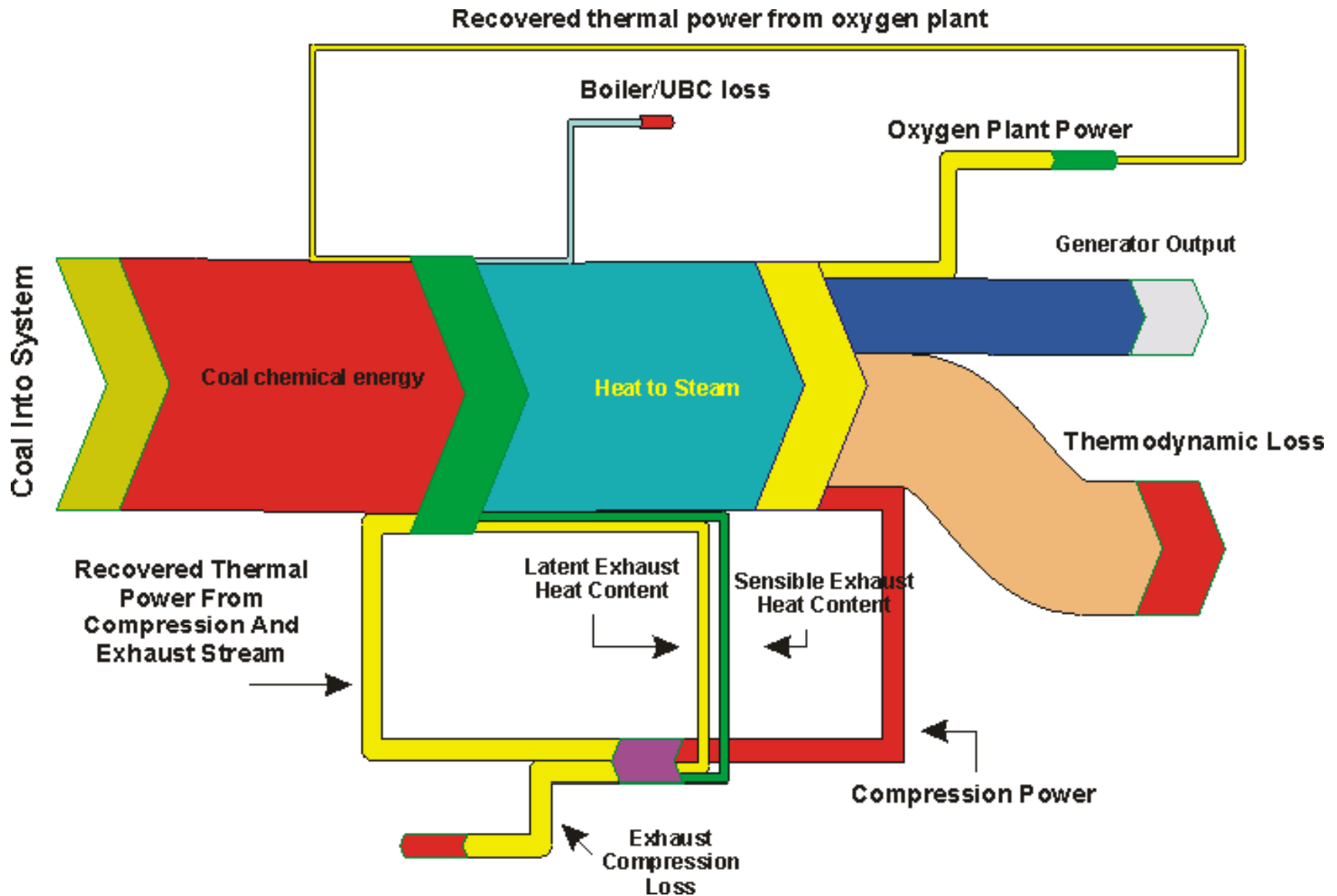


# Oxy-Firing/IPR



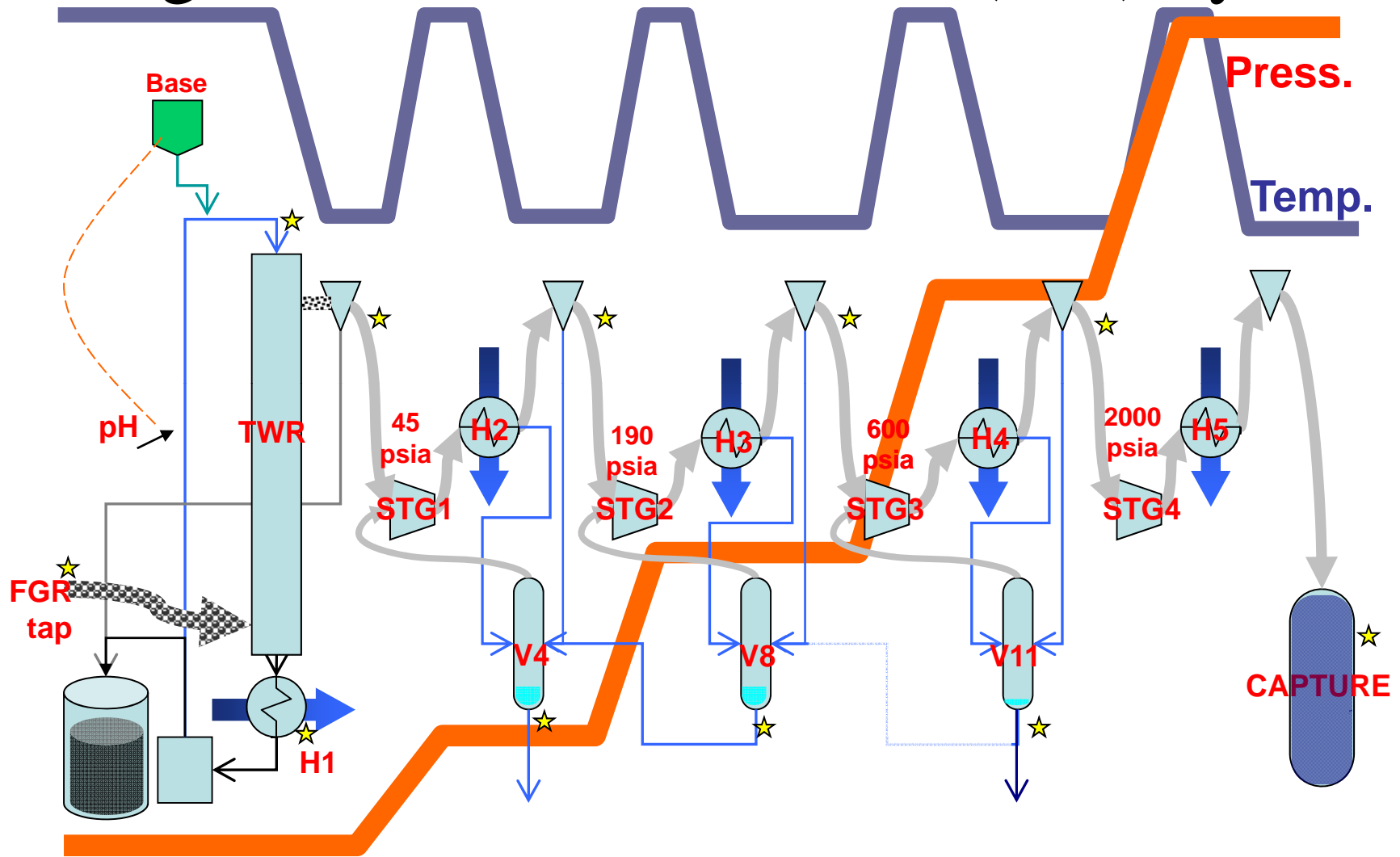
- Energy released in combustion is recovered through integration of feedwater heating and flue-gas cooling.
- Water is a by-product of this energy recovery.

# Oxy-Firing/IPR





# Integrated Pollutant Removal (IPR) System



# Water Opportunities

- Pollutants that now interact with atmospheric water are capturable from point-source liquid water
- Correctly applying recovered energy and water within the thermal cycle can maximize fuel efficiency (more fully using the energy entering with the fuel)
- Flue-gas water massflow offsets massflow of water required for thermal power production

# Questions for research

- Highly-efficient purification processes for released water
- Optimal full-use applications for recovered water
- Economic opportunities for material recovered during water purification

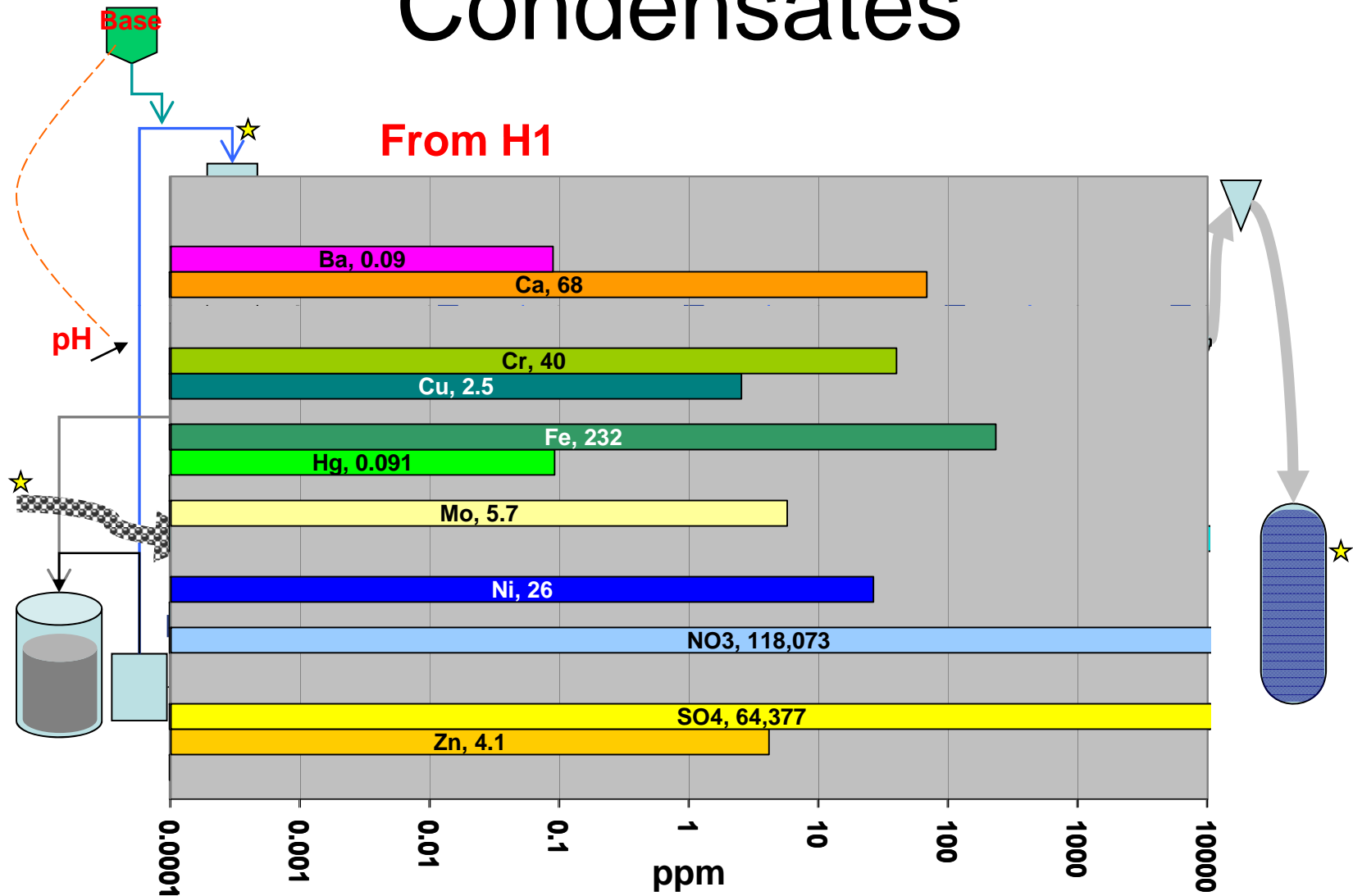
# What we are finding in IPR

- May be able to use less water in **Flue-Gas Desulphurization (FGD)**
  - Sulfur capture effective at pressure
- Species reporting at intercooler locations

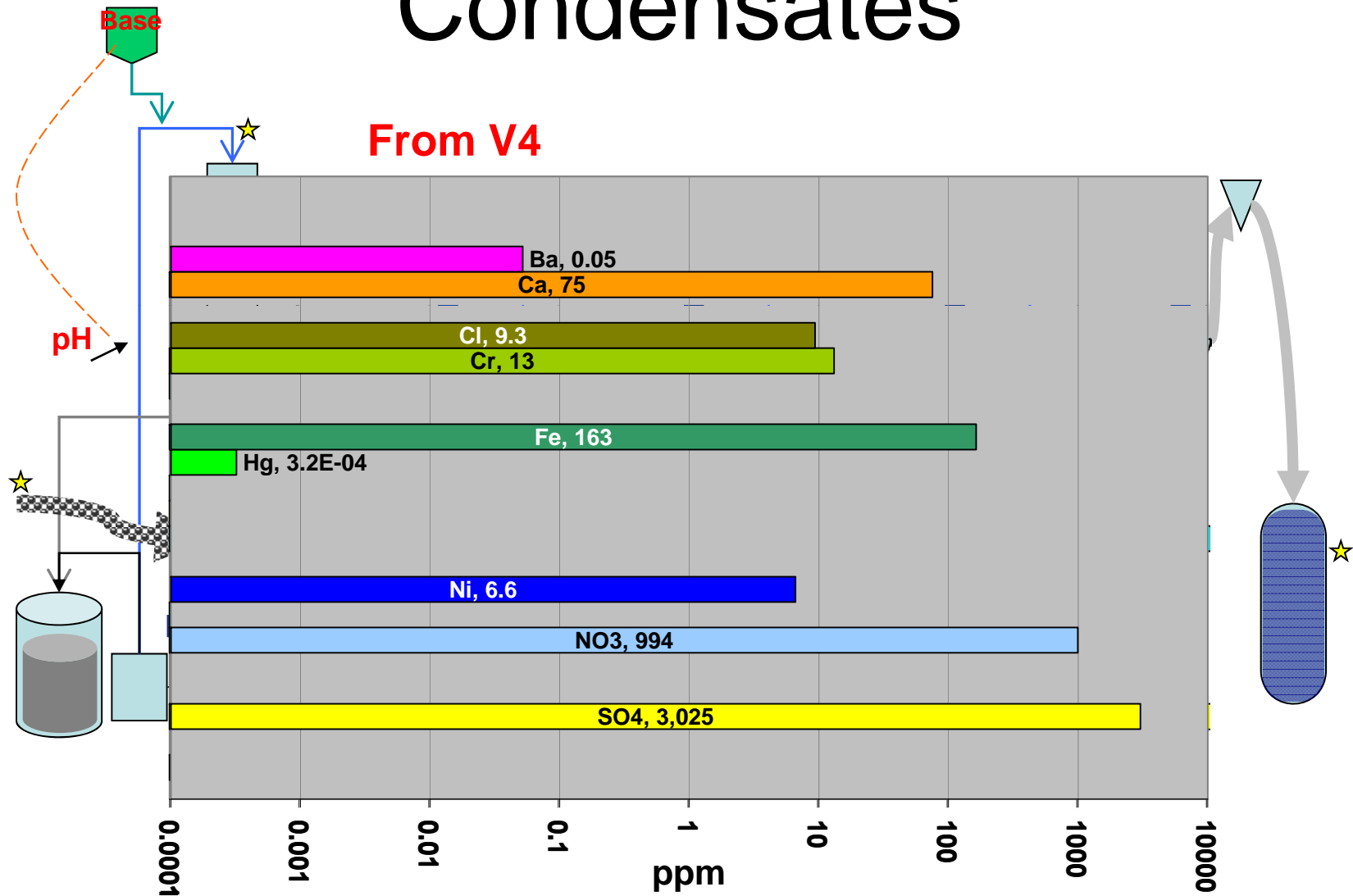
# Installation in the Field



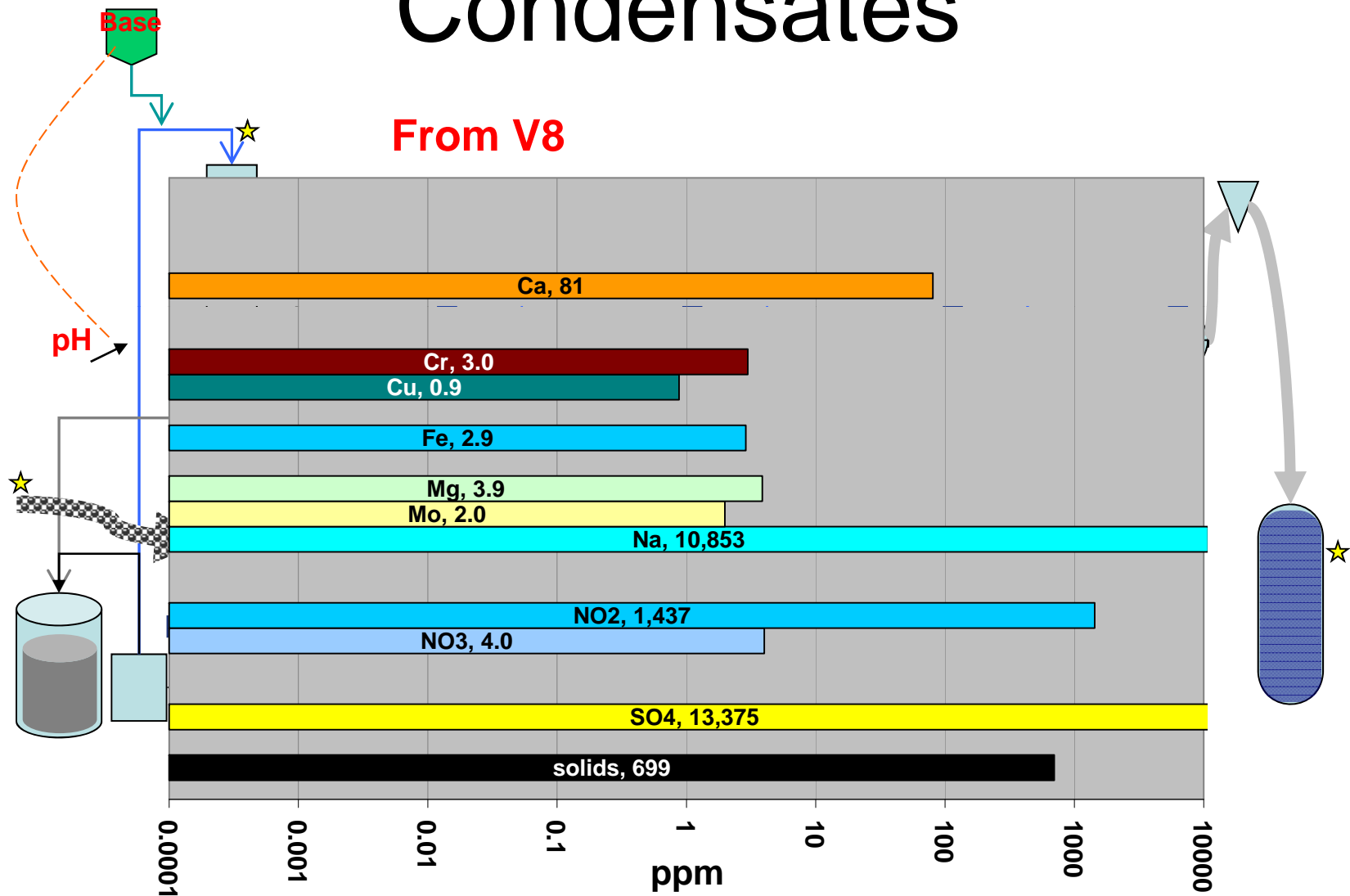
# Recovering Water – Process Condensates



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# Recovering Water – Process Condensates





# One Possible Approach

- Combustion products, entraining fine particulate (not caught in cyclone) sent counter-current to flue-gas-water spray to remove the bulk of the particles left.
  - Scrubber may employ bases to react with the SO<sub>x</sub> if needed.

# One Possible Approach

- The scrubber traps gas constituents that are water soluble as well as chemicals that leach out of the particles trapped in the scrubber.
  - Particles trapped by the scrubber are filtered out.
  - Scrubber water → Treat for reuse as spray

# One Possible Approach

- Treatment for water-offset applications
  - pH-swing precipitation and filtration
  - Demineralization (using ion exchange resins)
  - Testing for usage
  - Reuse in the cooling loop (IPR, or Plant at large)
  - Release

# Summary

- Recovering energy leads to recovering water
- Water removes pollutants from CO<sub>2</sub>
- Chemically adjusting water for thermal-cycle application
- Preventing release of those pollutants with returned water

Thank you for your attention.

# Exhaust Composition

	Conventional after economizer	Oxyfuel exhaust after splitter	After 1 <sup>st</sup> compression	After 2 <sup>nd</sup> compression	After 3 <sup>rd</sup> compression
Gas Flow (kg/hr)	1,716,395	409,083	364,367	354,854	353,630
Vol flow (m <sup>3</sup> /hr)	1,932,442	483,092	72,623	15,944	661
Inlet Pressure (psia)	14.62	15.51	62	264	1,500
Inlet Temperature (°F)	270	500	342	323	88.2
Density (kg/m <sup>3</sup> )	0.8882	0.8468	5.017	22.26	534.6
H <sub>2</sub> O (fraction)	0.0832	0.3322	0.0695	0.00994	0.0004
Ar (fraction)	0.0088	0.0115	0.0163	0.01730	0.0175
CO <sub>2</sub> (fraction)	0.1368	0.6131	0.8662	0.92161	0.9305
N <sub>2</sub> (fraction)	0.7342	0.0090	0.0128	0.01359	0.0137
O <sub>2</sub> (fraction)	0.0350	0.0250	0.0353	0.03755	0.0379
SO <sub>2</sub> (fraction)	0.0020	0.0091	0.0000	0.00000	0.0000